## Capacity Increase of Urea Plants



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### Outline

- o Targets and requirements of a revamp
- o Revamp concept for a capacity increase of 17% (1925-2250 MTPD)
- o Contractor's input
- o CO<sub>2</sub> generation



#### Targets and requirements of a revamp

- Capacity increase
  - By using existing margins to get maximum possible additional product with the lowest effort necessary
  - Elemination of bottlenecks
- Reduction of energy consumption (e.g. heat integration)
- o Environmental improvements
  - Reduction of emissions (to comply with new laws and international standards)
- o Increase of reliability and availability
- Utilization of a well proven and reliable technical concept
- Short as possible implementation downtime for modifications and new equipment



## Revamp targets

#### Melt Plant

Granulation

actual design

revamp

actual design

revamp



STAC + ~17% 2250 MTPD

UFT + 12.5% 2250 MTPD

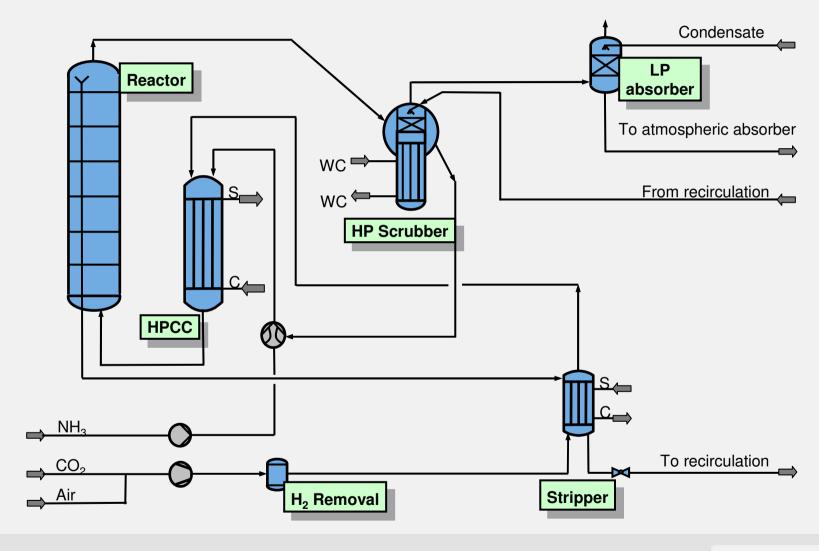


STAC + ~17% 2250 MTPD

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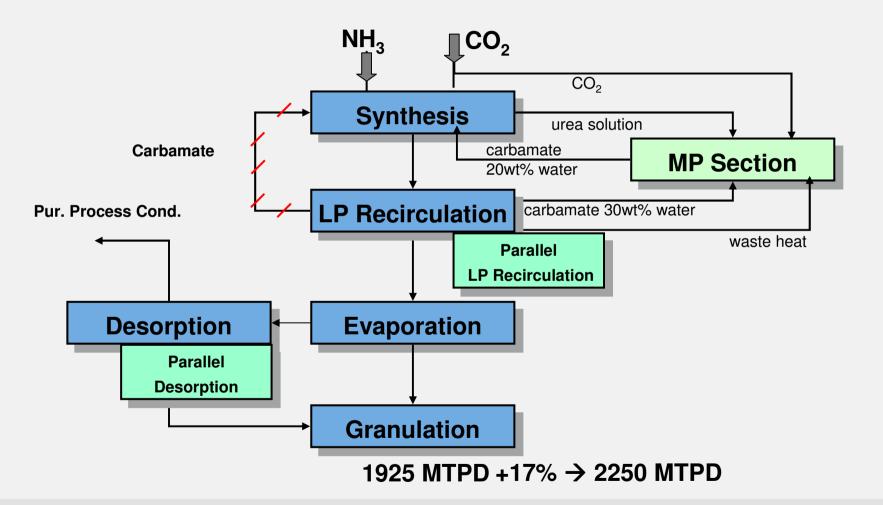


# The basis before the revamp for both plants Conventional *Stamicarbon* CO<sub>2</sub> Stripping Process



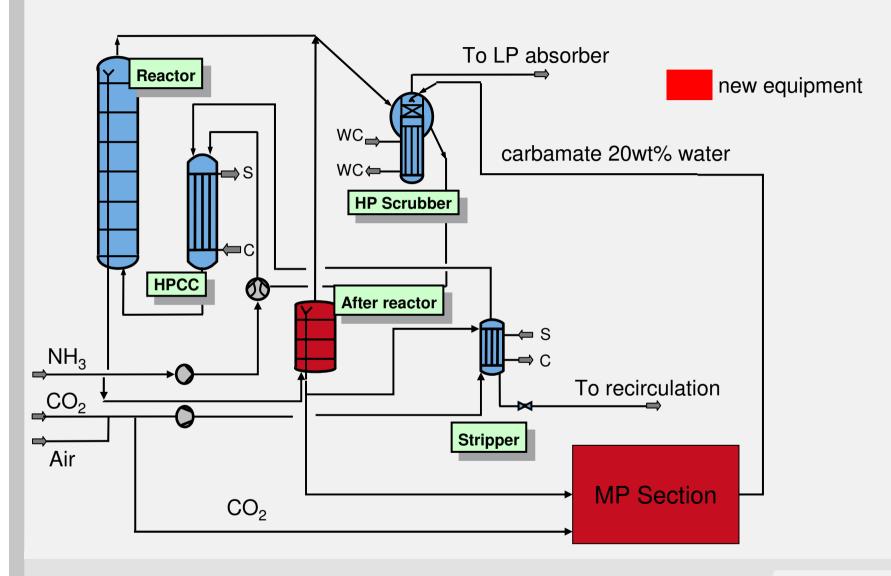


## Block Diagram Plant I & II (MP Section)

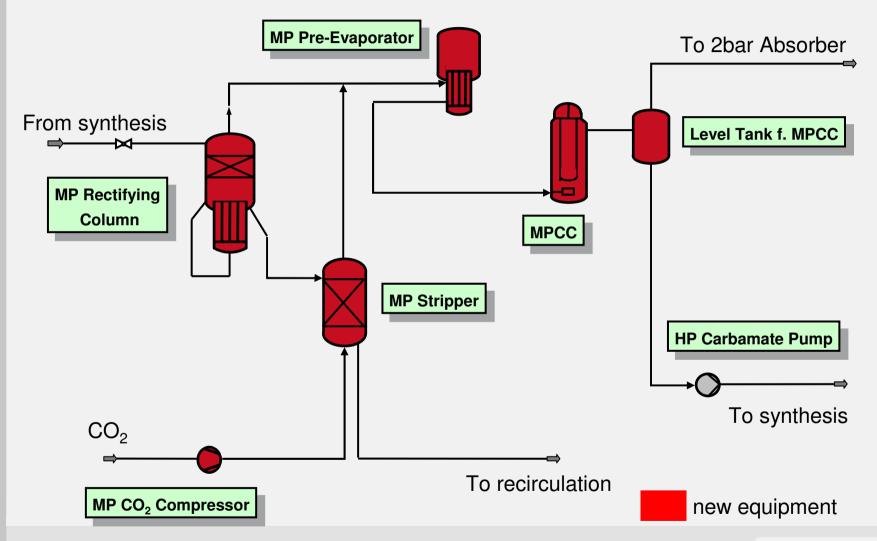




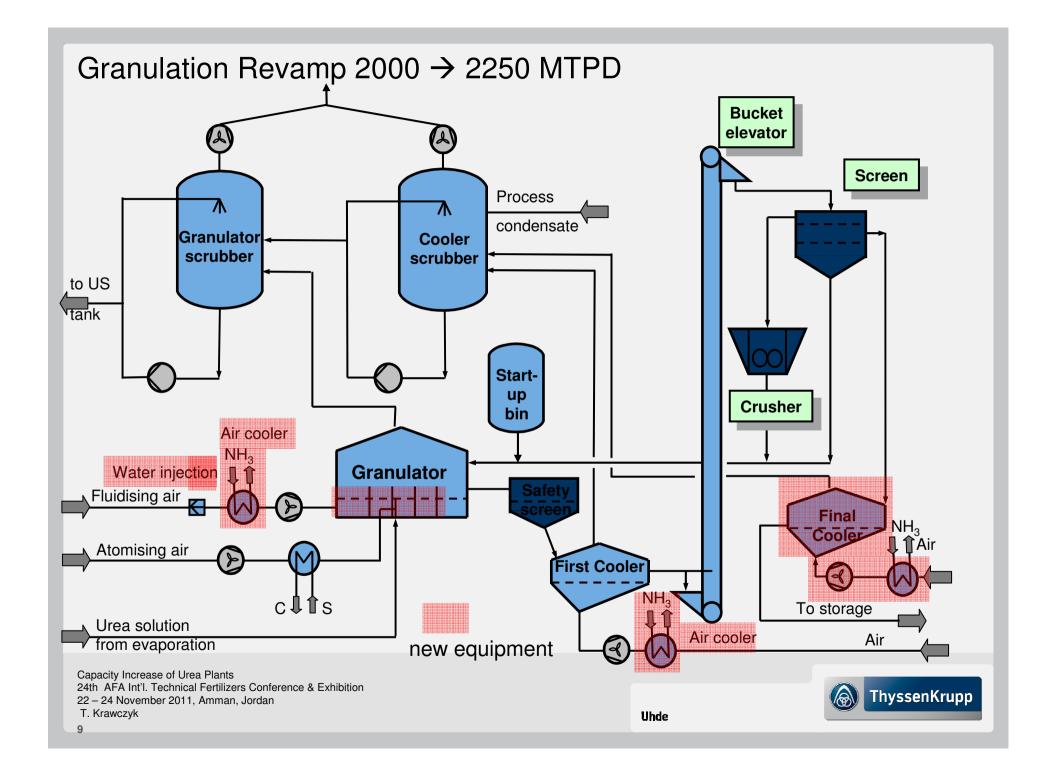
## Revamp concept 1925 → 2250 MTPD



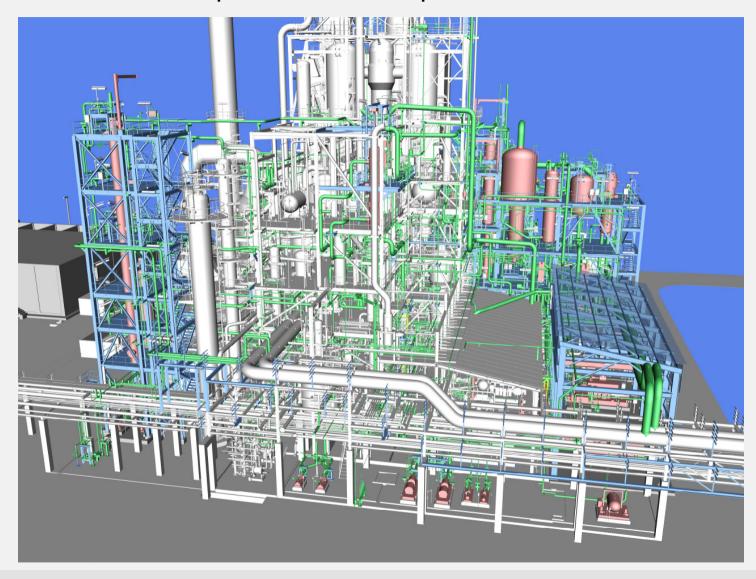
## MP Section (operating at ~20bar)





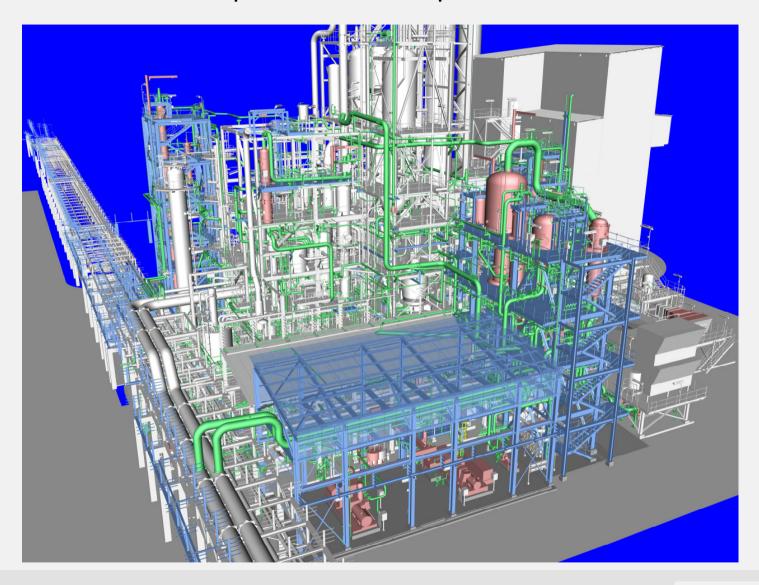


## Overview of the revamp measures for plant I & II





# Overview of the revamp measures for plant I & II



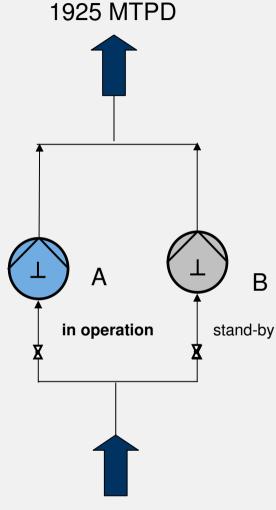




## Uhde's input to optimise the concept

Case 1: before revamp

- One pump in operation
- One pump stand-by



HP NH<sub>3</sub> / Carbamate Pumps





## Uhde's input to optimise the concept

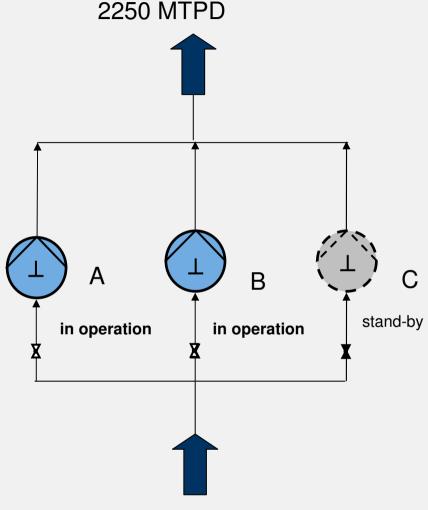
Case 2a: after revamp

Two pumps in operation

 Fall back to capacity before revamp in case of malfunction or maintenance

Case 2b: after revamp

- Two pumps in operation
- One pump stand-by
- Production remains at revamp capacity

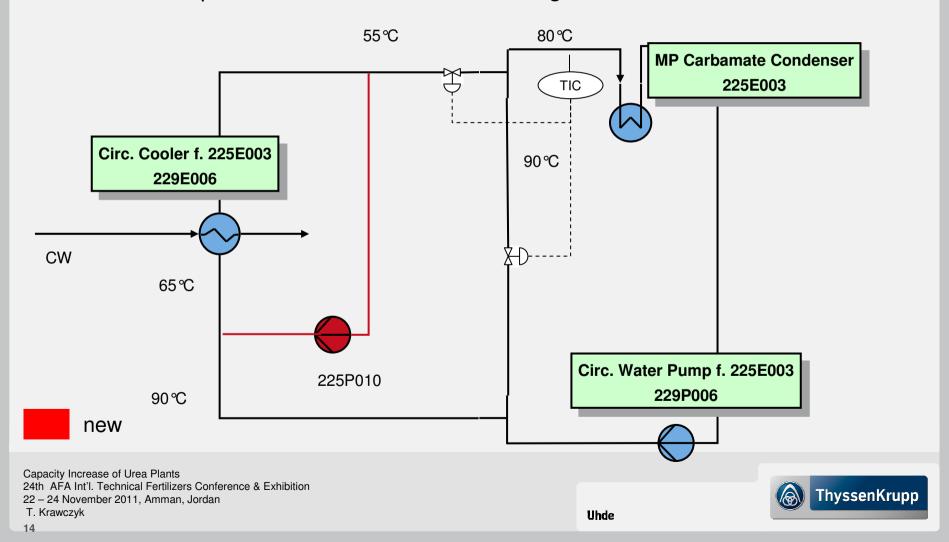


HP NH<sub>3</sub> / Carbamate Pumps



## Uhde's modifications of closed cooling water loops

Lower water temperature in order to reduce fouling on CW side.

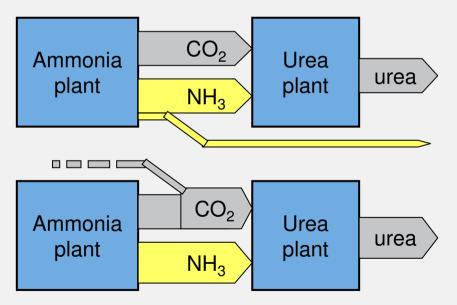


## CO<sub>2</sub> and NH<sub>3</sub> for Urea Production

Production of ammonia plant is typically with lower ratio CO2 / NH3
(1.14 t/t for ideal process with no loss and pure CH4 as feedstock)

o Demand of urea plant per ton of urea: 0.566 t NH<sub>3</sub> + 0.733 t CO<sub>2</sub>

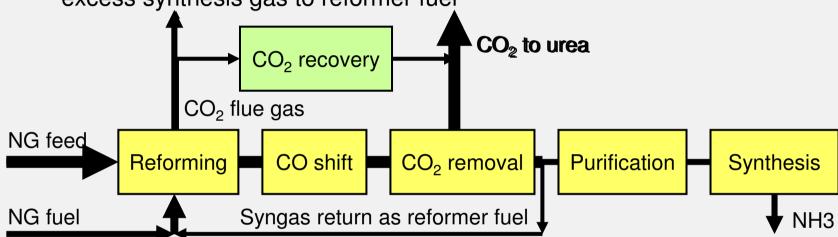
⇒Ratio CO<sub>2</sub> / NH<sub>3</sub> needed: 1.29 t/t





## Ways of CO<sub>2</sub> Production

o Staresæed/2002 porized Potices by inecrosæes y obthrough port to the Ozer emoval and return of excess synthesis gas to reformer fuel



#### Conclusion

- Changes in one place always lead to changes in another place
  - Overall knowledge
- Many constraints in an existing plant and set by the existing periphery
  - Collaboration between all involved parties
- Input to optimize the revamp concept for a tailor-made solution
  - Expierenced contractor

### Thank you for your attention!

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